

Dynamical systems and Control

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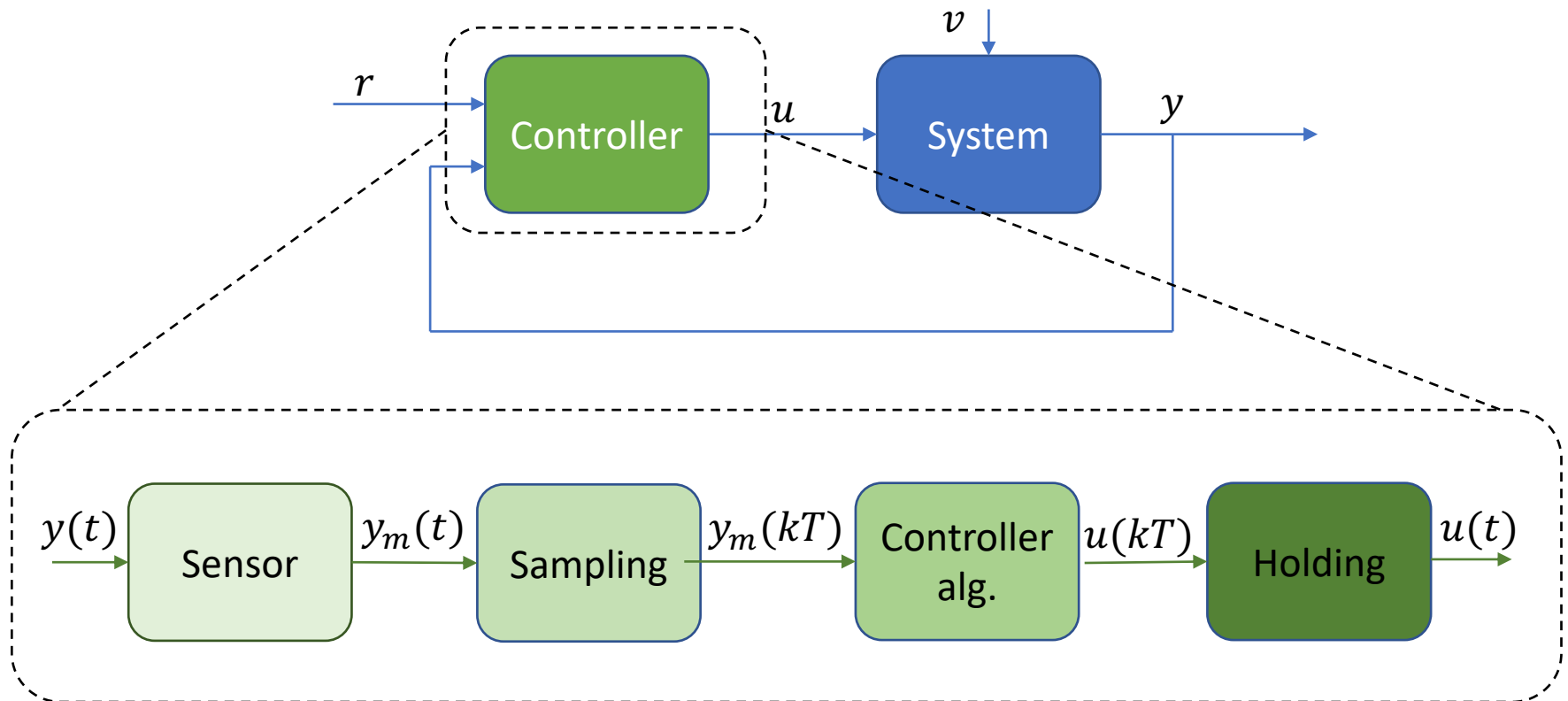
Lecture 6: Feedback

- Recap
- Open-loop vs. closed-loop control
- PID controller
- Analysis of the closed-loop system

Recap

A quick recap of lectures 1-5

A typical control loop

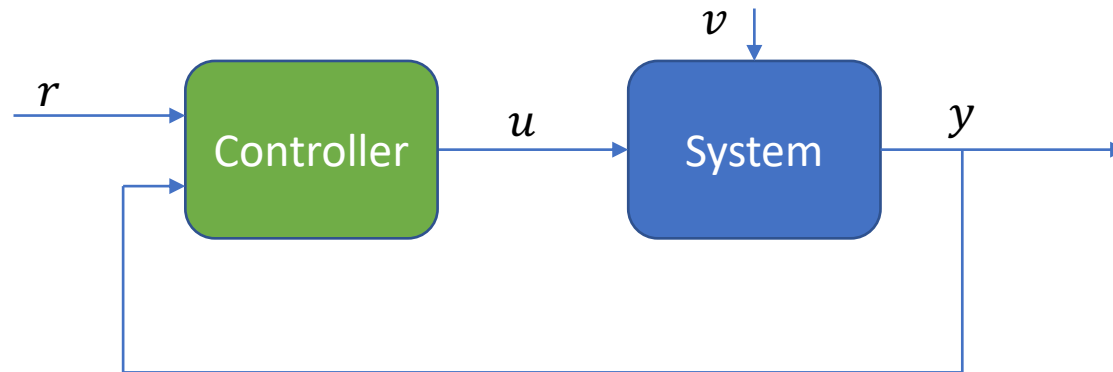


Controller

Concept

Open-loop vs. closed-loop controllers

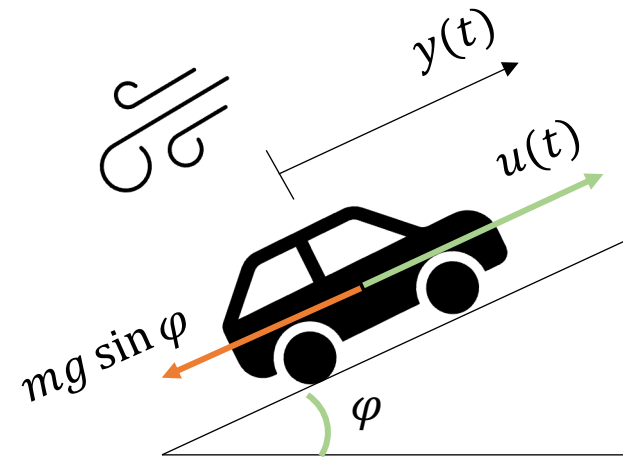
Concept



Example

The desired velocity $r(t) = 25 \text{ m/s}$. How to select $u(t)$?

Solution:



$u(t)$: Driving force

$F_a = ay(t)$: Air resistance force

$y(t)$: Velocity

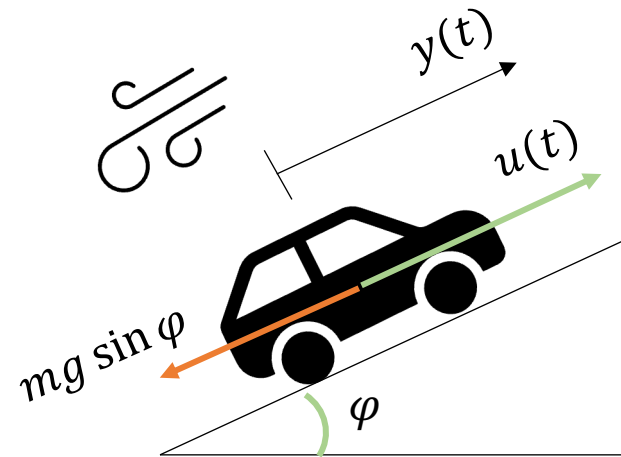
$mg \sin \varphi$: Disturbance

Example

Let $m = 1000 \text{ kg}$, $\alpha = 200 \text{ N s/m}$. The desired velocity $r(t) = 25 \text{ m/s}$. How to select $u(t)$?

Solution:

$$m\dot{y}(t) = u - mg \sin \varphi - \alpha y(t)$$



$u(t)$: Driving force

$F_a = \alpha y(t)$: Air resistance force

$y(t)$: Velocity

$mg \sin \varphi$: Disturbance

Example-Continued

Open-loop controller:

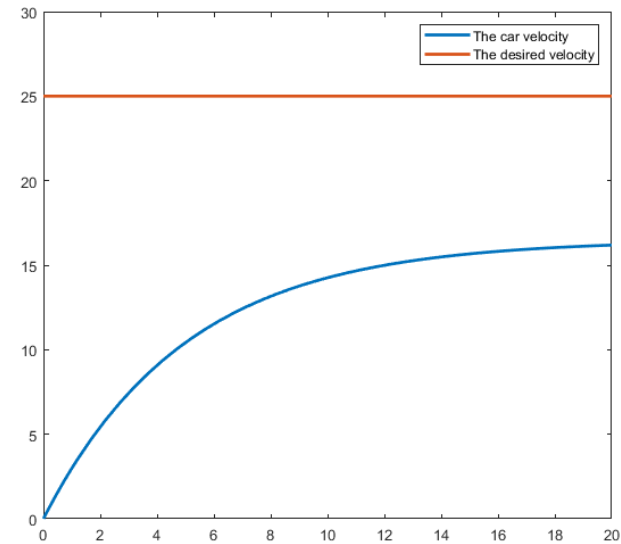
Example-Continued

Open-loop controller:

Set $y = r$ and $\dot{y} = 0$. We don't know the disturbance, so we design for $\varphi = 0$

$$u = \alpha r$$

But if $\varphi \neq 0$, we get the following plot, (here $\varphi = 10^\circ$)



Open-loop control

This strategy is called open-loop control:

- The performance is bad in general
- Not good if we have disturbance
- Not good if we don't know the model
- No freedom

What do we miss?

Example-Continued

Closed-loop controller:

Let's use the velocity $y(t)$.

Define the error

$$e(t) = r(t) - y(t)$$

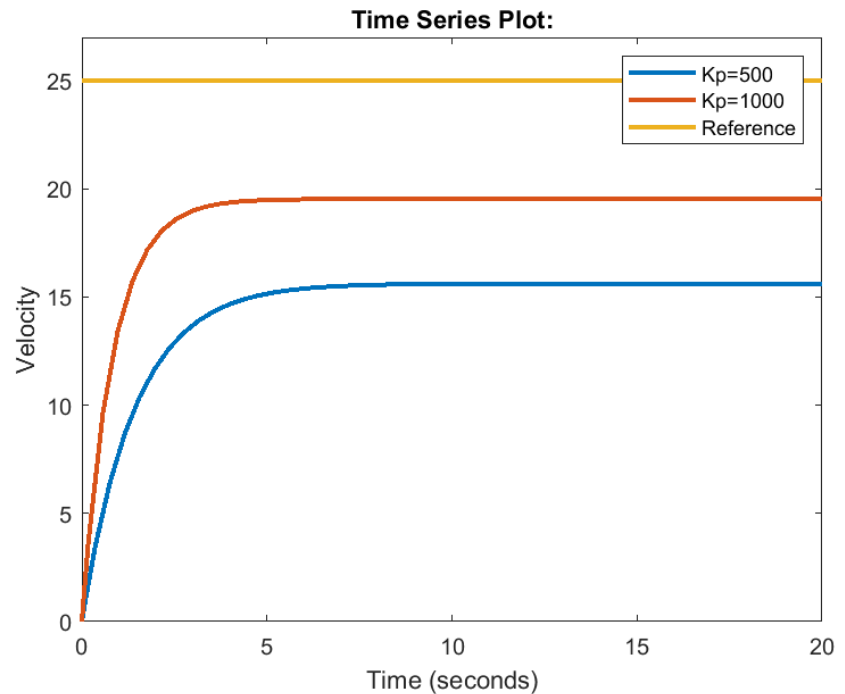
Select $u(t) = f(e(t))$

PID controller

Proportional (P):

$$u(t) = K_P e(t)$$

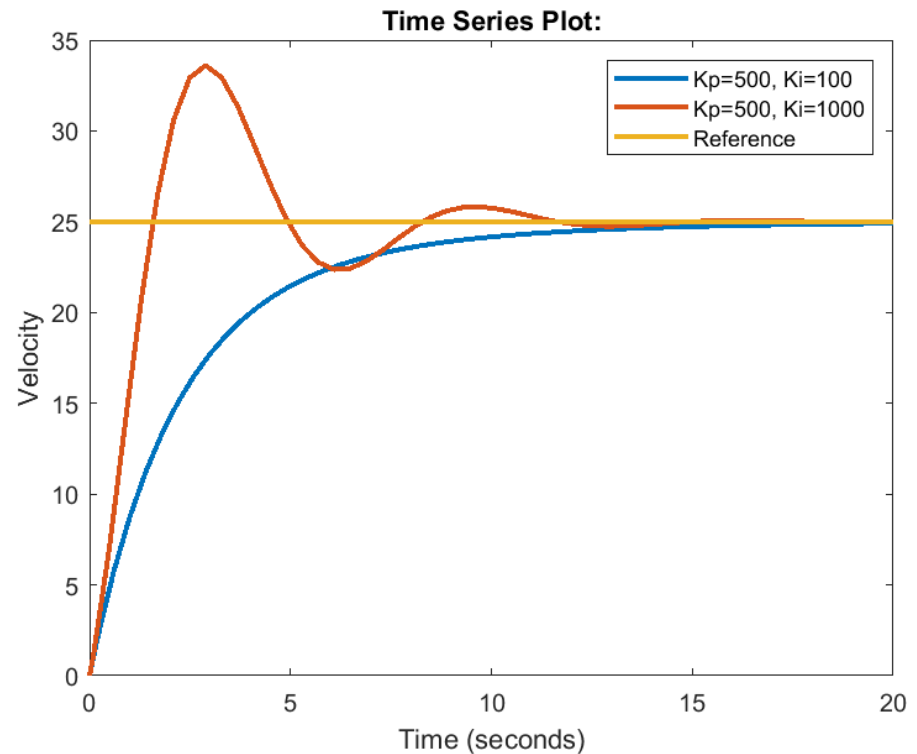
In the example: Bigger K_P , less error. But we cannot track the reference



Proportional-Integrator (PI):

$$u(t) = K_P e(t) + K_I \int_0^t e(\tau) d\tau$$

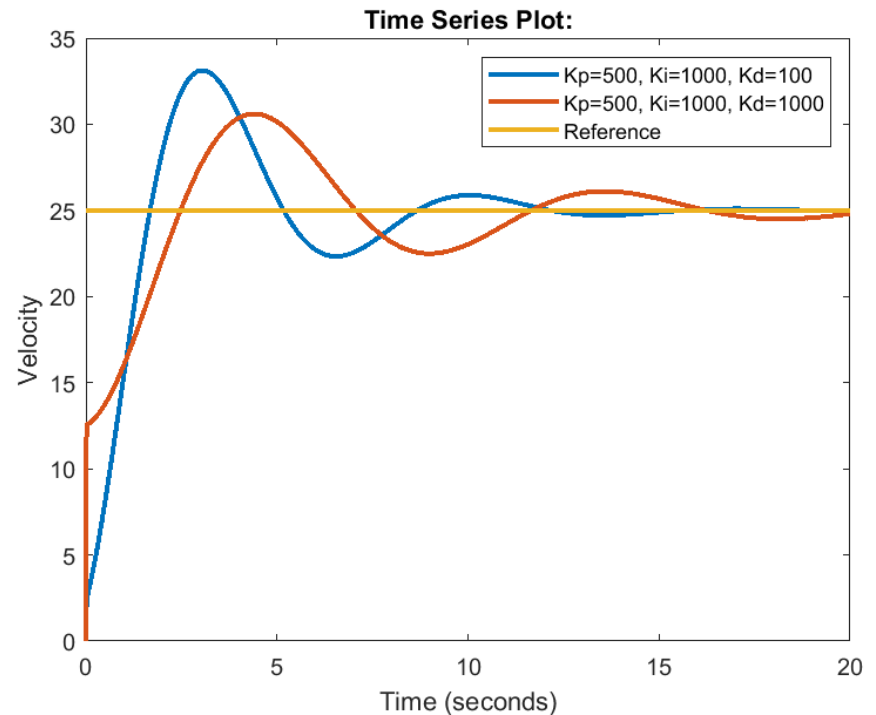
In the example: no error. But big values of K_I leads to oscillation and instability



Proportional-Integrator-Derivative (PID):

$$u(t) = K_P e(t) + K_I \int_0^t e(\tau) d\tau + K_D \dot{e}(t)$$

Add a derivative term,
predict the future



Summary

- P:*
- Big K_P :
 - Less permanent error
 - Big control effort
 - Can cause oscillation
- I:*
- Eliminate permanent error
 - Can cause oscillation, overshoot and instability
- D:*
- Reduce oscillation and overshoot
 - Sensitive to measurement noise

Analysis of the closed-loop system

Laplace transformation of PID

$$P: u(t) = K_P e(t)$$

$$PI: u(t) = K_P e(t) + K_I \int_0^t e(\tau) d\tau$$

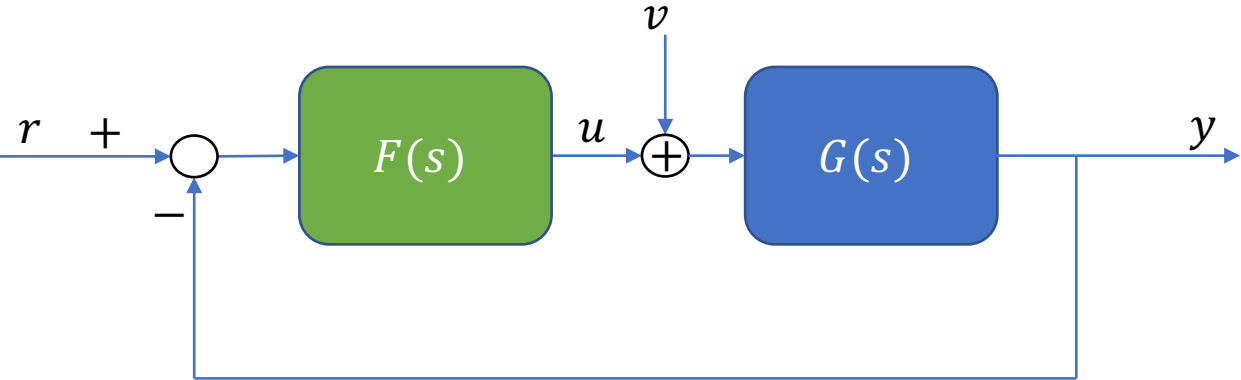
$$PID: u(t) = K_P e(t) + K_I \int_0^t e(\tau) d\tau + K_D \dot{e}(t)$$

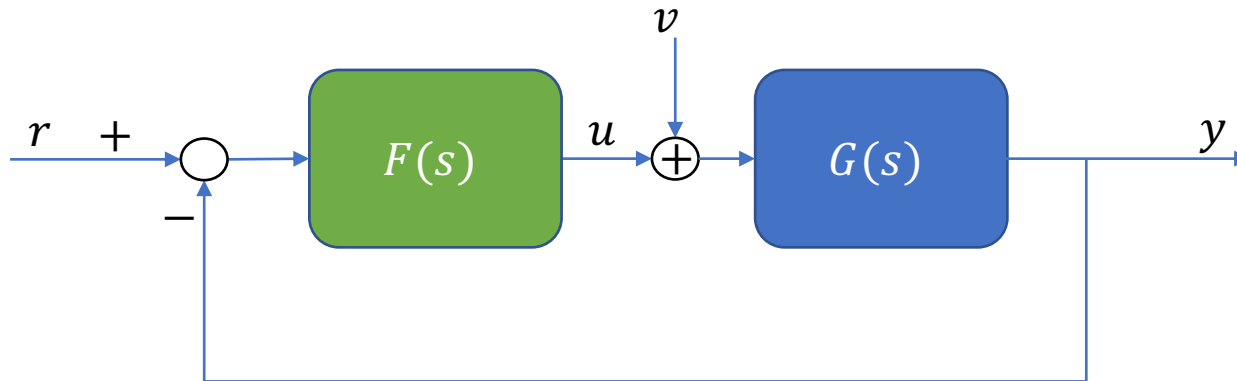
Laplace transformation of PID

$$P: u(t) = K_P e(t) \longrightarrow U(s) = K_P E(s)$$

$$PI: u(t) = K_P e(t) + K_I \int_0^t e(\tau) d\tau \longrightarrow U(s) = \left(K_P + \frac{K_I}{s}\right) E(s)$$

$$PID: u(t) = K_P e(t) + K_I \int_0^t e(\tau) d\tau + K_D \dot{e}(t) \longrightarrow U(s) = \left(K_P + \frac{K_I}{s} + K_D s\right) E(s)$$





$$Y(s) = G(s)(U(s) + V(s))$$

$$U(s) = F(s)E(s) = F(s)(R(s) - Y(s))$$

Replace the second equation in the first one

$$Y(s) = G(s)F(s)R(s) - G(s)F(s)Y(s) + G(s)V(s)$$

$$Y(s)(1 + G(s)F(s)) = G(s)F(s)R(s) + G(s)V(s)$$

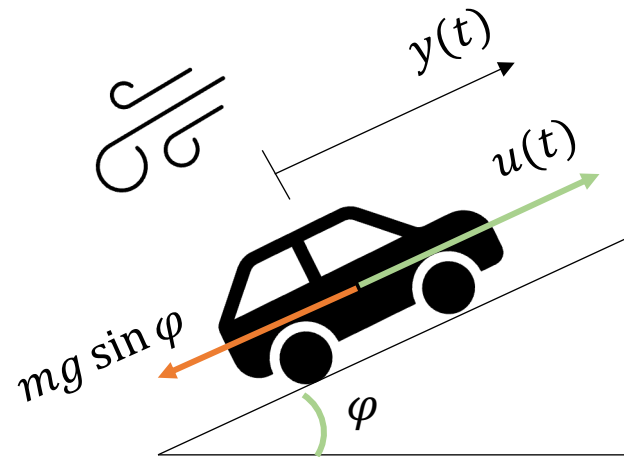
$$Y(s) = \frac{F(s)G(s)}{1 + F(s)G(s)}R(s) + \frac{G(s)}{1 + F(s)G(s)}V(s)$$

Example

Study stability when there is no disturbance and we use a P controller.

Solution:

$$m\dot{y}(t) = u - mg \sin \varphi - \alpha y(t)$$



Example

Study stability when there is no disturbance and we use a P controller.

Solution:

$$m\dot{y}(t) = u - \alpha y(t)$$

The transfer function of the system

$$G(s) = \frac{1/m}{s + \alpha/m}$$

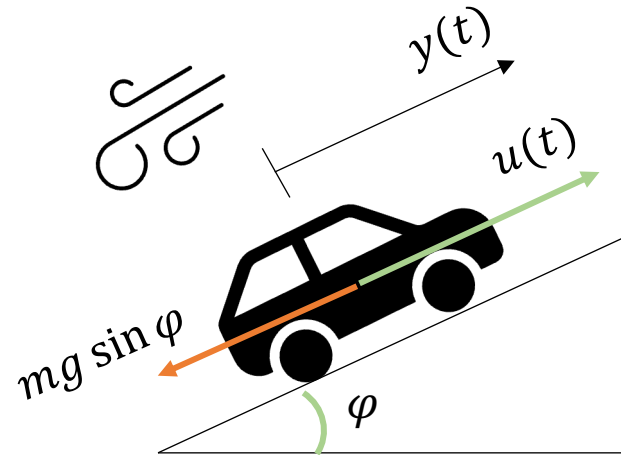
The transfer function of the controller

$$F(s) = K_p$$

The transfer function of the closed-loop system

$$G_c = \frac{F(s)G(s)}{1 + F(s)G(s)} = \frac{K_p \frac{1/m}{s + \alpha/m}}{1 + K_p \frac{1/m}{s + \alpha/m}} = \frac{K_p/m}{s + \alpha/m + K_p/m}$$

$\lambda = -\left(\frac{\alpha}{m} + \frac{K_p}{m}\right)$: is stable for all positive K_p



What do we cover next?

- Feedback issues
- Systems that are difficult to control
- PID tuning for simple systems

Ask us!

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